## The Clausius-Clapeyron Equation

Consider the following vapor pressure versus temperature data for the four liquids, water, benzene $\left(\mathrm{C}_{6} \mathrm{H}_{6}\right)$, acetone $\left(\left(\mathrm{CH}_{3}\right)_{2} \mathrm{CO}\right)$, and pentane $\left(\mathrm{C}_{5} \mathrm{H}_{12}\right)$.

|  | $0^{\circ} \mathrm{C}$ | $25^{\circ} \mathrm{C}$ | $50^{\circ} \mathrm{C}$ | $75^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{H}_{2} \mathrm{O}$ | 4.579 torr | 23.76 torr | 92.51 torr | 289.1 torr | 760.0 torr |
| $\mathrm{C}_{6} \mathrm{H}_{6}$ | 26.3 torr | 95.2 torr | 271.3 torr | 647.8 torr | 1350 torr |
| $\left(\mathrm{CH}_{3}\right)_{2} \mathrm{CO}$ | 70.14 torr | 230.9 torr | 614.3 torr | 1392 torr |  |
| $\mathrm{C}_{5} \mathrm{H}_{12}$ | 191.9 torr | 531.9 torr | 1231 torr |  |  |

When these data are plotted with the vapor pressure on the $y$-axis and temperature on the $x$-axis, the following graphs are obtained.

Pentane Acetone Benzene Water


These curves are actually exponential curves with the general form of

$$
\begin{equation*}
P=A\left(e^{-\Delta H / R T}\right) \tag{Eq.1}
\end{equation*}
$$

where P is the vapor pressure, $\Delta \mathrm{H}$ is the molar heat of vaporization, R is the gas constant which has a value of $8.314 \mathrm{~J} / \mathrm{mol} \cdot \mathrm{K}, \mathrm{T}$ is the temperature in kelvins, and A is a proportionality constant which varies from liquid to liquid.

A straight-line plot can be achieved if the logarithmic form of the above equation is used. That is, if the natural logarithm $(\ln )$ is taken of both sides of the above equation, the following is obtained.

$$
\begin{equation*}
\ln (P)=\ln (A)+\ln \left(e^{-\Delta H / R T}\right)=\ln (A)-\frac{\Delta H}{R T} \tag{Eq.2}
\end{equation*}
$$

Equation 2 may be easily rewritten in terms of common logarithms (i.e. logarithms in base 10) since,

$$
\begin{equation*}
\frac{\ln (P)}{2.303}=\log (P) \tag{Eq.3}
\end{equation*}
$$

Thus, if equation 2 is divided by 2.303 and then the term "log" substituted for the term "ln/2.303", the following equation is obtained in terms of common logarithms.

$$
\begin{equation*}
\log (P)=\log (A)-\frac{\Delta H}{2.303 R T}=-\frac{\Delta H}{2.303 R}\left(\frac{1}{T}\right)+\log (A) \tag{Eq.4}
\end{equation*}
$$

It should be noted that equation 4 has the general form of a linear equation: $y=m x+b$.


Thus, if the common logarithm of the vapor pressure $(\log P)$ is plotted on the $y$-axis and the reciprocal of the temperature $(1 / T)$ is plotted on the $x$-axis, a straight line graph is achieved with a slope of $-\Delta H / 2.303 \mathrm{R}$. Using the above data and equation 4 the following graphs are obtained. Equation 4 . is one form of the Clausius-Clapeyron Equation. The use of this equation requires the knowledge of the value of the constant $A$, which varies from liquid to liquid. However, if vapor pressure data are available at two different temperatures then an alternative form of the Clausius-Clapeyron Equation may be derived which does not require the constant A .

Since,

$$
\begin{equation*}
\log \left(P_{1}\right)=-\frac{\Delta H}{2.303 R} \quad\left(\frac{1}{T_{1}}\right)+\log (A) \tag{Eq.5}
\end{equation*}
$$

where $P_{1}$ is the vapor pressure at temperature $T_{1}$, and

$$
\begin{equation*}
\log \left(P_{2}\right)=-\frac{\Delta H}{2.303 R} \quad\left(\frac{1}{T_{2}}\right)+\log (A) \tag{Eq.6}
\end{equation*}
$$

where $P_{2}$ is the vapor pressure at temperature $T_{2}$,
the term, $\log (\mathrm{A})$, may be eliminated by subtracting the second equation from the first equation. I.e.

$$
\begin{equation*}
\log \left(P_{1}\right)-\log \left(P_{2}\right)=-\frac{\Delta H}{2.303 R}\left(\frac{1}{T_{1}}\right)+\frac{\Delta H}{2.303 R}\left(\frac{1}{T_{2}}\right)=\frac{\Delta H}{2.303 R}\left(\frac{1}{T_{2}}-\frac{1}{T_{1}}\right) \tag{Eq.7}
\end{equation*}
$$

Finally, by using the laws of logarithms, the usual form of the Clausius-Clapeyron Equation is obtained.

$$
\begin{equation*}
\log \left(\frac{P_{1}}{P_{2}}\right)=\frac{\Delta H}{2.303 R}\left(\frac{1}{T_{2}}-\frac{1}{T_{1}}\right)=\frac{\Delta H}{2.303 R}\left(\frac{T_{1}-T_{2}}{T_{2} T_{1}}\right) \tag{Eq.8}
\end{equation*}
$$

## Uses of the Clausius-Clapeyron Equation: (This equation can be used in three ways.)

1) To determine the heat of vaporization, $\Delta H$.

If vapor pressure data is known at two different temperatures (i.e., $\mathrm{T}_{1}, \mathrm{P}_{1}, \mathrm{~T}_{2}$, and $\mathrm{P}_{2}$ are known), then the molar heat of vaporization, $\Delta \mathrm{H}$, can be estimated. This is done by rearranging (Eq. 8) to solve for $\Delta \mathrm{H}$.

$$
\begin{equation*}
\Delta H=2.303 R\left(\frac{T_{2} T_{1}}{T_{1}-T_{2}}\right) \times \log \left(\frac{P_{1}}{P_{2}}\right) \tag{Eq.9}
\end{equation*}
$$

For example: The vapor pressure of pentane is 191.9 torr at $0^{\circ} \mathrm{C}(273.15 \mathrm{~K})$ and is 531.9 torr at $25^{\circ} \mathrm{C}(298.15 \mathrm{~K})$. The heat of vaporization, $\Delta \mathrm{H}$, of pentane is easily estimated by substituting these values into (Eq. 9).

$$
\begin{equation*}
\Delta H=2.303(8.314 \mathrm{~J} / \mathrm{mol} \cdot \mathrm{~K})\left(\frac{298.15 \mathrm{~K} \times 273.15 \mathrm{~K}}{273.15 \mathrm{~K}-298.15 \mathrm{~K}}\right) \log \left(\frac{191.9 \text { torr }}{531.9 \text { torr }}\right)=2.762 \times 10^{4} \mathrm{~J} / \mathrm{mol} \tag{Eq.10}
\end{equation*}
$$

## 2) To estimate the vapor pressure at a given temperature.

If the molar heat of vaporization, $\Delta \mathrm{H}$, has been determined and the vapor pressure $\left(\mathrm{P}_{1}\right)$ is known at a given temperature $\left(\mathrm{T}_{1}\right)$, then the vapor pressure $\left(\mathrm{P}_{2}\right)$ can be estimated at a second given temperature $\left(\mathrm{T}_{2}\right)$. This is done by rearranging (Eq.8) to solve for $\log \left(\mathrm{P}_{2}\right)$.
$\log \left(P_{2}\right)=\log \left(P_{1}\right)-\frac{\Delta H}{2.303 R}\left(\frac{1}{T_{2}}-\frac{1}{T_{1}}\right)=\log \left(P_{1}\right)-\frac{\Delta H}{2.303 R}\left(\frac{T_{1}-T_{2}}{T_{2} T_{1}}\right)=X$
then taking the antilog of this quantity to give $\mathrm{P}_{2}$.

$$
\begin{equation*}
P_{2}=\operatorname{antilog}(X) \tag{Eq.12}
\end{equation*}
$$

For example: The vapor pressure of water is 23.8 torr at $25^{\circ} \mathrm{C}$ and the heat of vaporization of water is $43.56 \mathrm{~kJ} / \mathrm{mol}$. The vapor pressure of water at $50^{\circ} \mathrm{C}$ can be estimated by substituting the given quantities into (Eq.11) and calculating $\log \left(\mathrm{P}_{2}\right)$.

$$
\begin{equation*}
\log \left(P_{2}\right)=\log (23.76 \text { torr })-\frac{43.56 \times 10^{3} \mathrm{~J} / \mathrm{mol}}{(2.303)(8.314 \mathrm{~J} / \mathrm{mol} \cdot \mathrm{~K})}\left(\frac{1}{323.15 \mathrm{~K}}-\frac{1}{298.15 \mathrm{~K}}\right)=1.9662 \tag{Eq.13}
\end{equation*}
$$

Then, $\mathrm{P}_{2}$ can be estimated by taking the antilog of 1.9662 .

$$
\begin{equation*}
P_{2}=\operatorname{antilog}(1.9662)=92.51 \text { torr } \tag{Eq.14}
\end{equation*}
$$

3) To estimate the temperature where the liquid exerts a given vapor pressure.

If the molar heat of vaporization, $\Delta \mathrm{H}$, has been determined and the vapor pressure $\left(\mathrm{P}_{1}\right)$ is known at a given temperature $\left(\mathrm{T}_{1}\right)$, then the temperature $\left(\mathrm{T}_{2}\right)$ can be estimated where a liquid has a second given vapor pressure $\left(\mathrm{P}_{2}\right)$. This is done by rearranging (Eq.8) to solve for $\left(1 / \mathrm{T}_{2}\right)$.

$$
\begin{equation*}
\frac{1}{T_{2}}=\frac{2.303 R}{\Delta H} \times \log \left(\frac{P_{1}}{P_{2}}\right)+\left(\frac{1}{T_{1}}\right)=X \tag{Eq.15}
\end{equation*}
$$

then, taking the reciprocal of X gives $\mathrm{T}_{2}$.
For example: The vapor pressure of water is 23.8 torr at $25^{\circ} \mathrm{C}$ and the heat of vaporization of water is $43.56 \mathrm{~kJ} / \mathrm{mol}$. The temperature at which the vapor pressure of water is 40.00 torr can be estimated by substituting these quantities into (Eq.15) and calculating the quantity ( $1 / \mathrm{T}_{2}$ ).

$$
\begin{equation*}
\frac{1}{T_{2}}=\frac{(2.303)(8.314 \mathrm{~J} / \mathrm{mol} \cdot \mathrm{~K})}{43.56 \times 10^{3} \mathrm{~J} / \mathrm{mol}} \times \log \left(\frac{23.76 \text { torr }}{40.00 \mathrm{torr}}\right)+\left(\frac{1}{298.15 \mathrm{~K}}\right)=0.003255 \mathrm{~K}^{-1} \tag{Eq.16}
\end{equation*}
$$

Taking the reciprocal of $0.003255 \mathrm{~K}^{-1}$ gives $\mathrm{T}_{2}$.

$$
\begin{equation*}
T_{2}=\left(\frac{1}{0.003255 K^{-1}}\right)=307.2 \mathrm{~K}=34.0^{\circ} \mathrm{C} \tag{Eq.17}
\end{equation*}
$$

